

# PAR elevation influence study

F.Dabbene

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### Context



## • Containment Thermalhydraulics during severe accident

- Containment initialy filled with Air (50 to 80000 m3)
- Before core degradation:
  - Hot steam released into the containment (jet/plume)
  - Bulk condensation and wall condensation in presence of noncondensible gases (Air)
  - Natural or mixed convection flows
- Core degradation:
  - Hydrogen (reduction of steam by Zircaloy claddings) released into the containment (with or without steam)
  - H2 risk

#### Principle of Passive Autocatalytic Recombiner (PAR)



- 1. Gas enters at the PAR bottom
- 2. Hydrogen contacts the plates
- 3. Catalytic reaction begins
- 4. Reaction heats the gas and the PAR housing
- 5. Gas rises and leaves at the top of the PAR
- 6. Natural convection takes place (pumping effect)

#### Outline





- PARIS benchmark
- Flow structure analysis
- PAR elevation influence

#### PARIS benchmark (SARNET, WP12.2)

- PAR elevation influence on hydrogen distribution: set the PAR at the half box elevation
- Natural convection loop interaction: one PAR on each side
- PAR is a SIEMENS FR90/1-150 like one  $\rm_{\rm H}$  (h=1m, w=0.2, 15 plates)
- SIEMENS H2 consumption (kg/s) given by *min(Xh2,Xo2,0.08)(Ap+B) with A=0.48E-8 and B=0.58E-3*
- Homogeneous initial mixture at 393K, saturated steam, dry Xh2=5% and air mass the one at 1bar and 298K
- No heat and mass transfer through walls





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#### Dry H2 molar fraction at t=60s and 600s



#### Pressure evolution and density at t=3000s



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#### Dry Xh2 at t=3000s



• No stratification only for the lower elevation (not shown, homogeneous dry hydrogen fraction of  $\approx$  1.3%)



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## Temperature (C) at t=3000s

 No stratification only for the lower elevation (not shown, homogeneous temperature of 272C





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#### Dry Xh2 at t=60s

 $\mathcal{C}$ 

 Lower the PAR elevation is, larger the hydrogen mobilization is, longer burning and mixing processes are



### Conclusion

• Fast H2 depletion rate but low mobilization below the PAR: an additional process is necessary to enhance mixing process and limit thermal and mass stratifications (wall heat and mass transfer, etc.)

- Code-to-code comparisons exhibit some differences:
  - For the transient phase, the flow pattern at the PAR outlet (plume or jet behaviour)
  - At the guasi steady-state, the floor layer diffusion
- Several interaction levels
  - PAR level (H2 consumption rate, plates/flow interactions)
  - Nearfield level (PAR/atmosphere interactions)
  - Farfield level (H2 distribution)
- Difficulties to deal with all space and time scales
  - Separate effect analysis is necessary
  - Farfield and nearfield connexions have to be understood
- Lack of experimental data

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- Lumped approaches of the KALI and H2PAR programs
- REKO (FzJ) dedicated to H2 consumption rate (plate interactions)
- In project or in progress, larger scale programs dedicated to CFD code: PANDA (SETHII) and REKO 4 (FzJ) for example

PARIS

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- Thanks for your attention

#### PAR inlet/outlet and LP temperature evolution with time

- No stratification only for the lower elevation (homogeneous, T=272°C)
- Higher the PAR elevation is, larger the thermal stratification is
- More than 50°C of inlet/outlet temperature differe nce for the transient
- Decreasing plate temperature with time due to decreasing of H2 consumption rate and mass flow rate through the PAR
- Left/right PAR symmetry is conserved



#### PAR mass flow rate and H2 mass evolution with time



• At the lower elevation, the hydrogen molar fraction goes below the threshold value of 0.5%. Thus, the H2 consumption rate goes to 0. So the mass flow rate because there is no more heat release.



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#### Velocity at t=60s

• Lower the PAR is, larger the hydrogen mobilization is





#### Dry Xh2 evolution along the left vertical line x=3w

• No stratification only for the lower elevation (homogeneous T of  $272^{\circ}$ )

• Higher the PAR elevation is, larger the mass stratification is

