

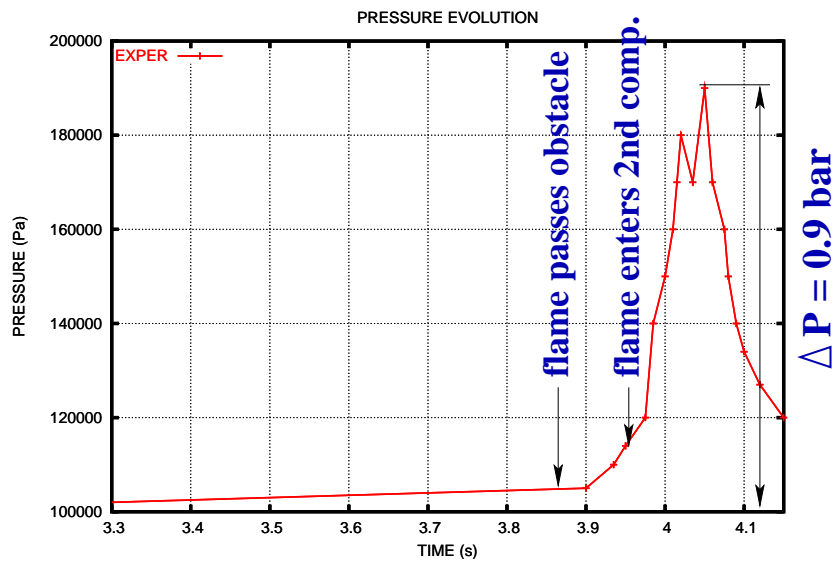
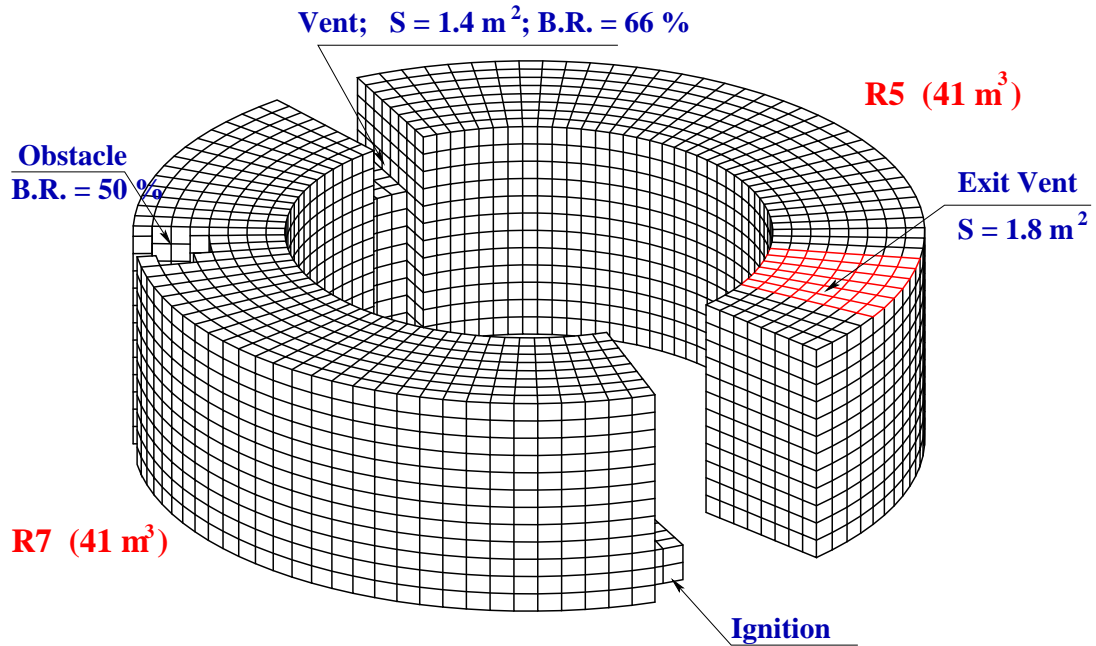
Club CASTEM 2004

November 26, 2004.

**Simulation of HDR and BMC Hydrogen
Combustion Tests with the TONUS code
and CREBCOM model.**

Hydrogen Deflagration Test Ex29 (BMC).

Initial conditions: 10 % H_2 , P = 1 bar, T = 337 K.



Governing Equations.

CREBCOM combustion model.

$$\frac{\partial \rho}{\partial t} + \vec{\nabla} \cdot (\rho \vec{u}) = 0 \quad (1)$$

$$\frac{\partial \rho Y_k}{\partial t} + \vec{\nabla} \cdot (\rho \vec{u} Y_k) = \rho \dot{\omega}_k \quad (2)$$

$$\frac{\partial \rho \vec{u}}{\partial t} + \vec{\nabla} \cdot (\rho \vec{u} \otimes \vec{u} + P\mathbf{I}) = \rho \vec{g} \quad (3)$$

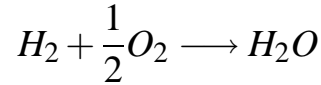
$$\frac{\partial \rho e_t}{\partial t} + \vec{\nabla} \cdot (\rho \vec{u} h_t) = \rho \vec{g} \cdot \vec{u} - \rho \sum_j h_j^0 \dot{\omega}_j - H(T - T_0) \quad (4)$$

$$\frac{\partial \rho K_0}{\partial t} + \vec{\nabla} \cdot (\rho \vec{u} K_0) = 0 \quad (5)$$

$$\frac{\partial \rho Y_{H_2,f}}{\partial t} + \vec{\nabla} \cdot (\rho \vec{u} Y_{H_2,f}) = 0 \quad (6)$$

$$\frac{\partial \rho Y_{H_2,i}}{\partial t} + \vec{\nabla} \cdot (\rho \vec{u} Y_{H_2,i}) = 0 \quad (7)$$

Where



$$\xi = \frac{Y_{H_2} - Y_{H_2,i}}{Y_{H_2,f} - Y_{H_2,i}}$$

$$\dot{\omega}_\xi = \frac{K_0}{\Delta x} \times \{criter.function\}$$

“Automatic” Determination of the parameter K_0

METHOD (I) Source: A.A. Efimenko and S.Dorofeev. CREBCOM code system for description of gaseous combustion (2001).

$$\mathbf{K}_0 = \frac{\sigma + 1}{4} \mathbf{S}_T = \frac{\mathbf{S}_T}{\mathbf{S}_L} \times \frac{\sigma + 1}{4} \mathbf{S}_L \quad (8)$$

Where

$$\begin{aligned} \frac{S_T}{S_L} &= 0.5(\sigma - 1) \left(\frac{L}{\delta} \right)^{1/3} Le^{-2/3} \quad \text{if } \frac{L}{\delta} > 500 \\ \frac{S_T}{S_L} &= 0.0008(\sigma - 1)^3 \left(\frac{L}{\delta} \right) \quad \text{if } \frac{L}{\delta} < 500 \\ L &= L_c \times \max(0.1; 0.5(1 - \sqrt{1 - BR})) \end{aligned}$$

METHOD (II) Source: S.Dorofeev and R. Redlinger. Description of FLAME3D (2003).

$$\mathbf{K}_0 = \frac{\sigma + 3}{8} \mathbf{S}_T = \frac{\mathbf{S}_T}{\mathbf{S}_L} \times \frac{\sigma + 3}{8} \mathbf{S}_L \quad (9)$$

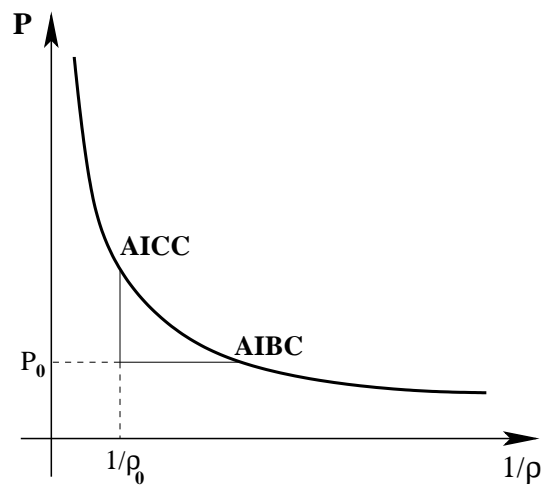
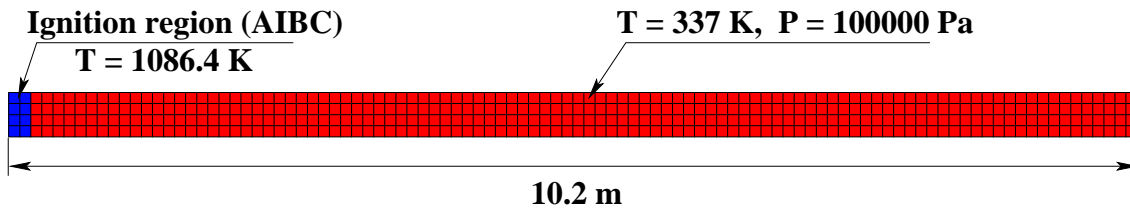
where

$$\frac{S_T}{S_L} \approx 30.0 \quad \text{for } V/S/dx \approx 6.0$$

METHOD (III) Source: P. Pailhories. Bilan des calculs de combustion multi-D réalisés avec le modèle CREBCOM du code TONUS (2003).

$$\mathbf{K}_0 = 66.7 \times \mathbf{S}_L \quad \text{for } V/S/dx \approx 2.0 \quad (10)$$

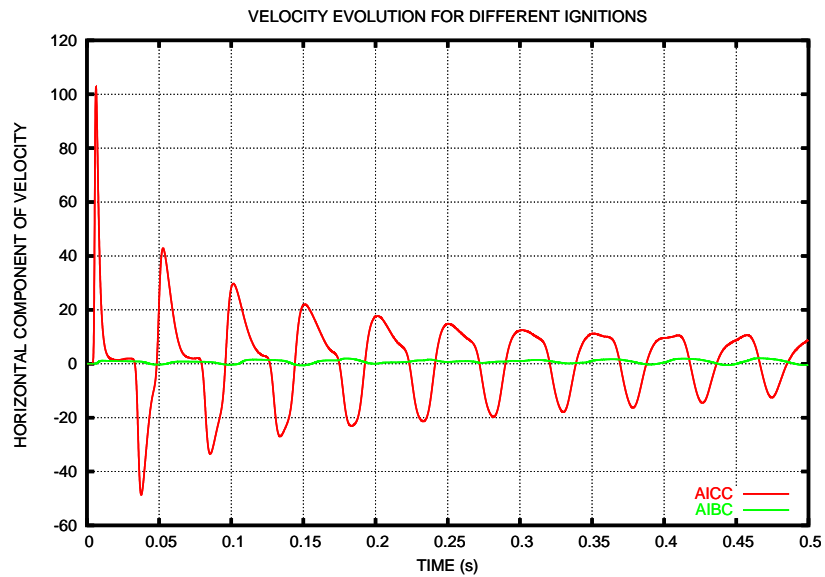
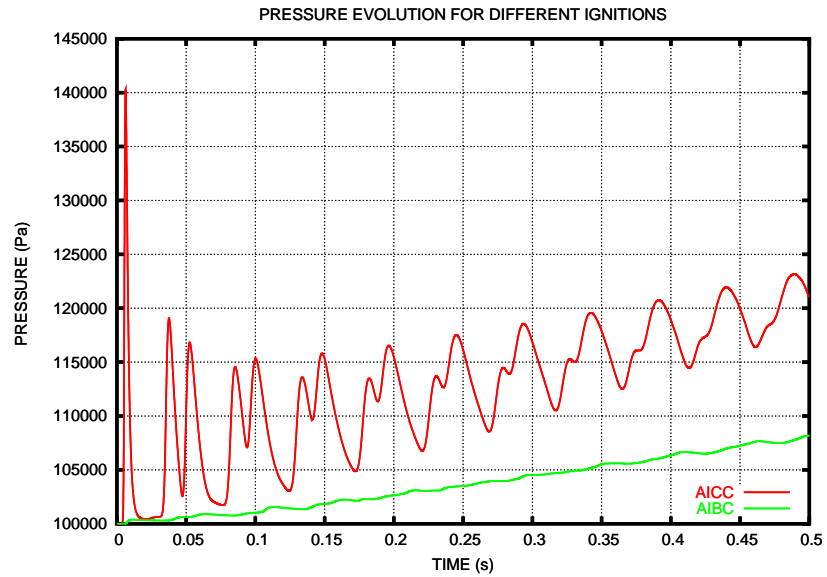
Presentation of the Ignition Problem



Two ways of ignition:

- **AICC** (Adiabatic Isochore Complete Combustion) $\rho_2 = \rho_1$;
($T \approx 1300 \text{ K}, P \approx 3.65 \times 10^5 \text{ Pa}$).
- **AIBC** (Adiabatic IsoBare complete Combustion) $P_2 = P_1$.
($T \approx 1086 \text{ K}$).

Pressure and velocity evolution at the capteur

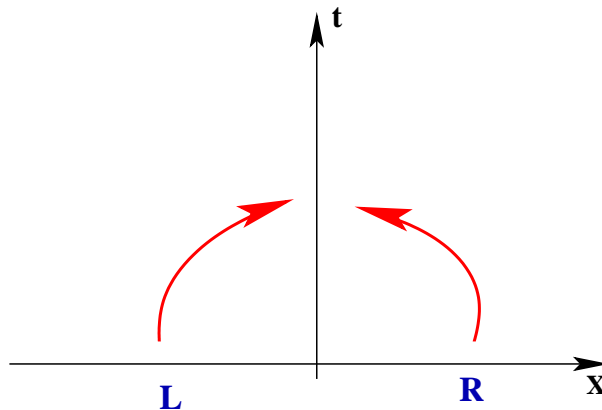


Choice of the Numerical Scheme (1)

a) Flux Vector Splitting scheme (VLH)

$$\mathbf{F}_{num}(\mathbf{U}_L, \mathbf{U}_R) = \mathbf{F}^+(\mathbf{U}_L) + \mathbf{F}^-(\mathbf{U}_R) \quad (11)$$

Stationary contact line is diffused.



b) Flux Difference Splitting scheme (SS)

$$\mathbf{F}_{num}(\mathbf{U}_L, \mathbf{U}_R) = \mathbf{F}(RP(0; \mathbf{U}_L, \mathbf{U}_R)) \quad (12)$$

Stationary contact line is resolved.

Choice of the Numerical Scheme (2)

1D results.

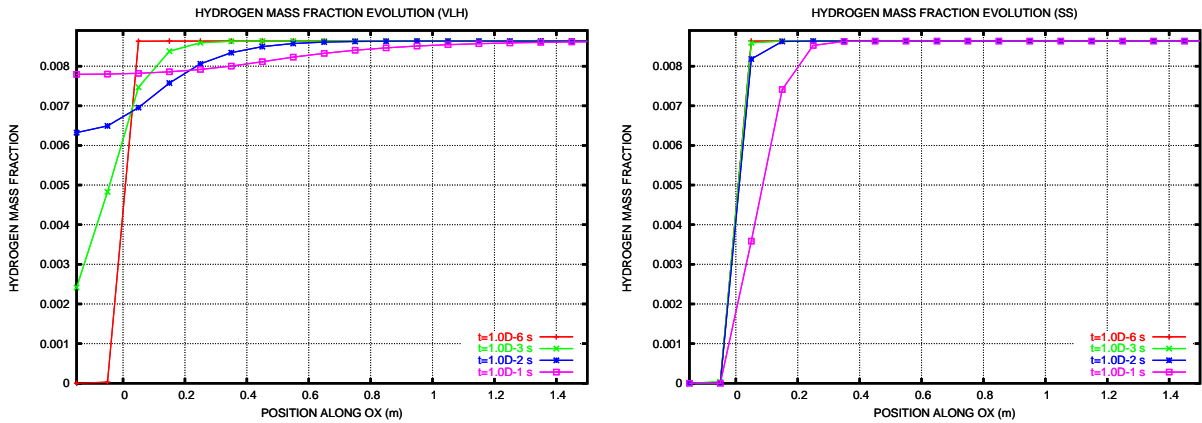


Figure 1: Hydrogen Mass Fraction Evolution using VLH scheme (left) and SS scheme (right)

2D results.

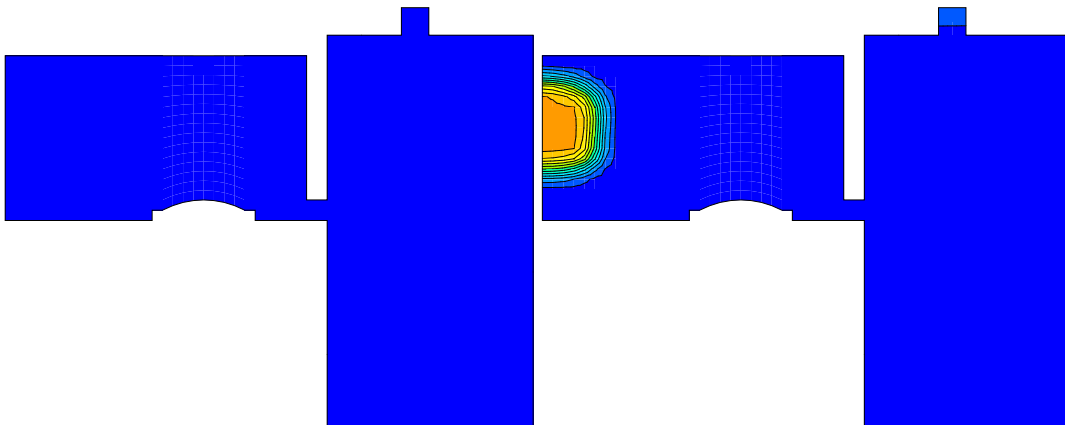
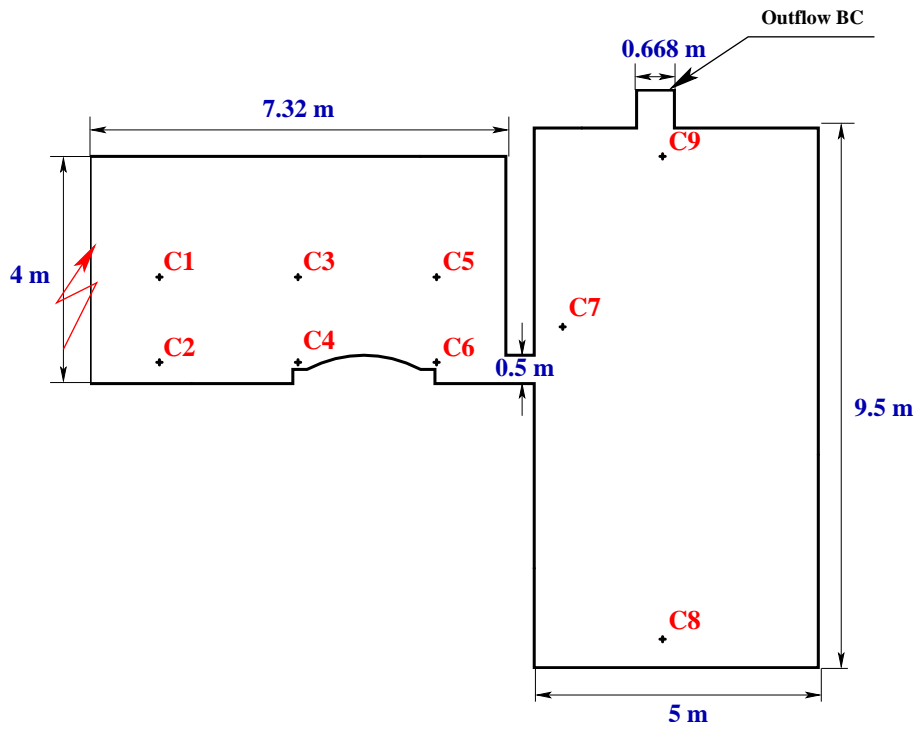


Figure 2: Temperature isolines at $t = 1.0$ s using VLH(2nd order) scheme (left) and SS(2nd order) scheme (right). ΔT between isolines is 62.75 K.

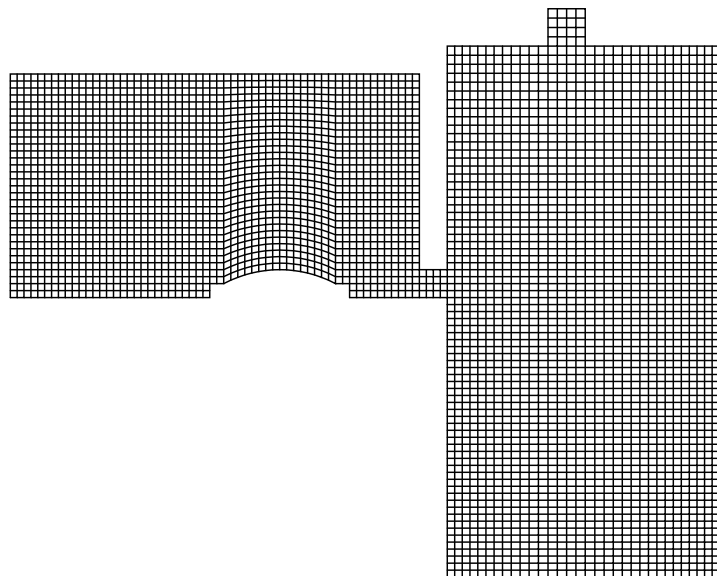
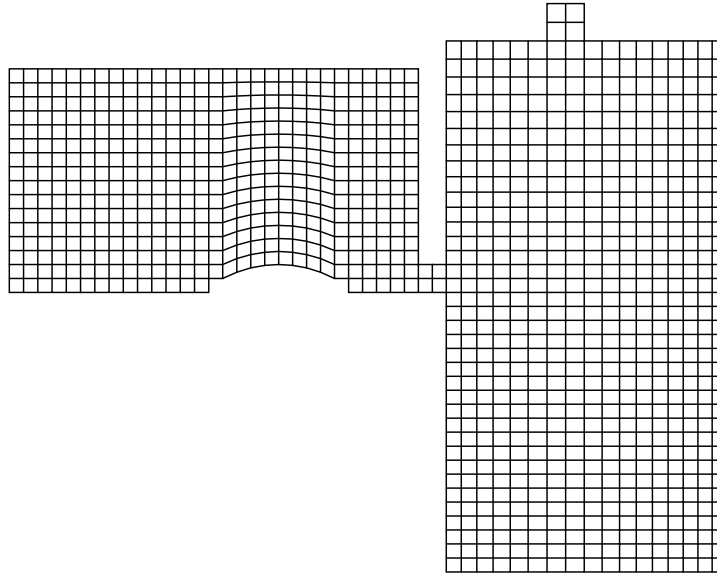
E12.3.2 computation using 2D geometry.



Method	R1904	R1905	R1801
I	7.48	7.48	11.08
II	9.38	9.38	9.38
III	18.9	18.9	18.9
2D, present comp.	0.41	0.41	3.7
3D, present comp.	0.55	0.55	2.8

Table 1: **HDR Test E12.3.2.** Values of K_0 computed using different methods.

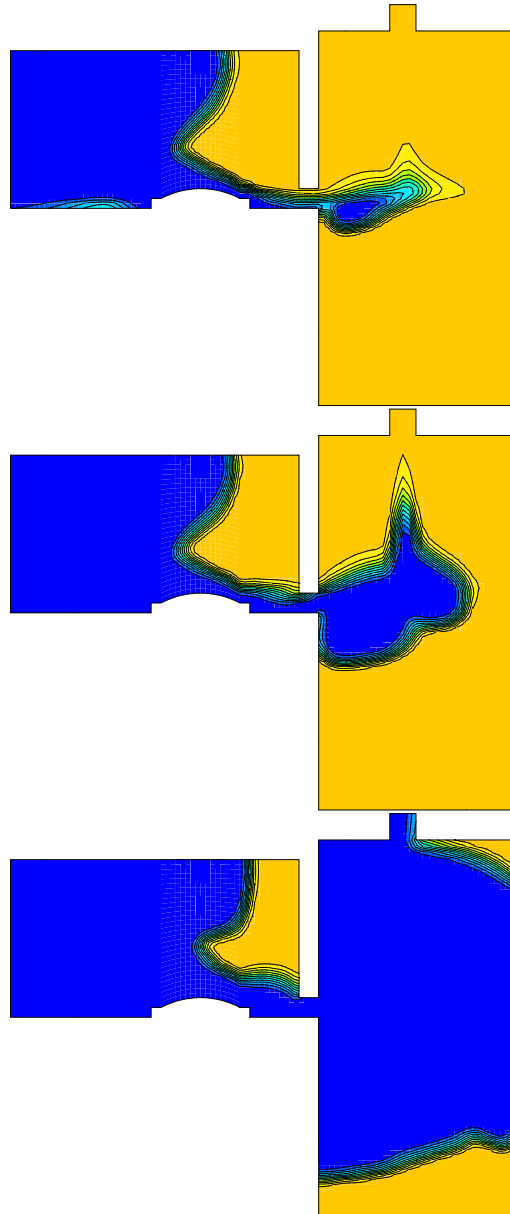
E12.3.2 computation. Mesh of 1074 and 4256 elements



2D version of the E12.3.2 computation.

Hydrogen Mass Fraction Evolution. Fine Mesh.

$t = 2.4 \text{ s}, t = 2.5 \text{ s}$ and $t = 2.9 \text{ s}$



Pressure evolutions. Effect of the Grid Refinement.

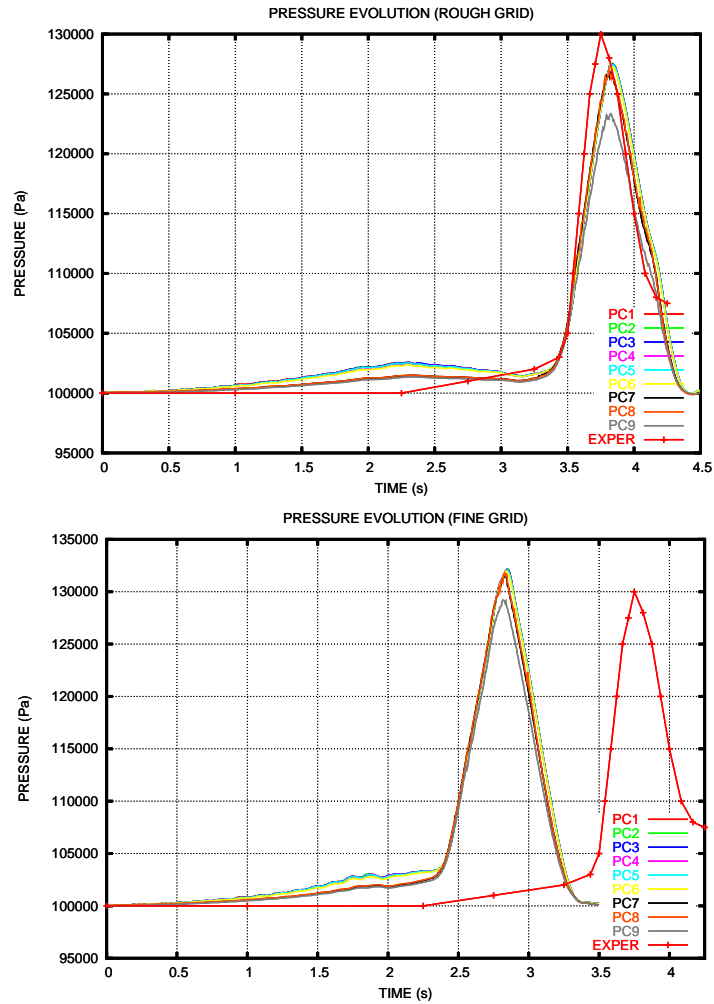
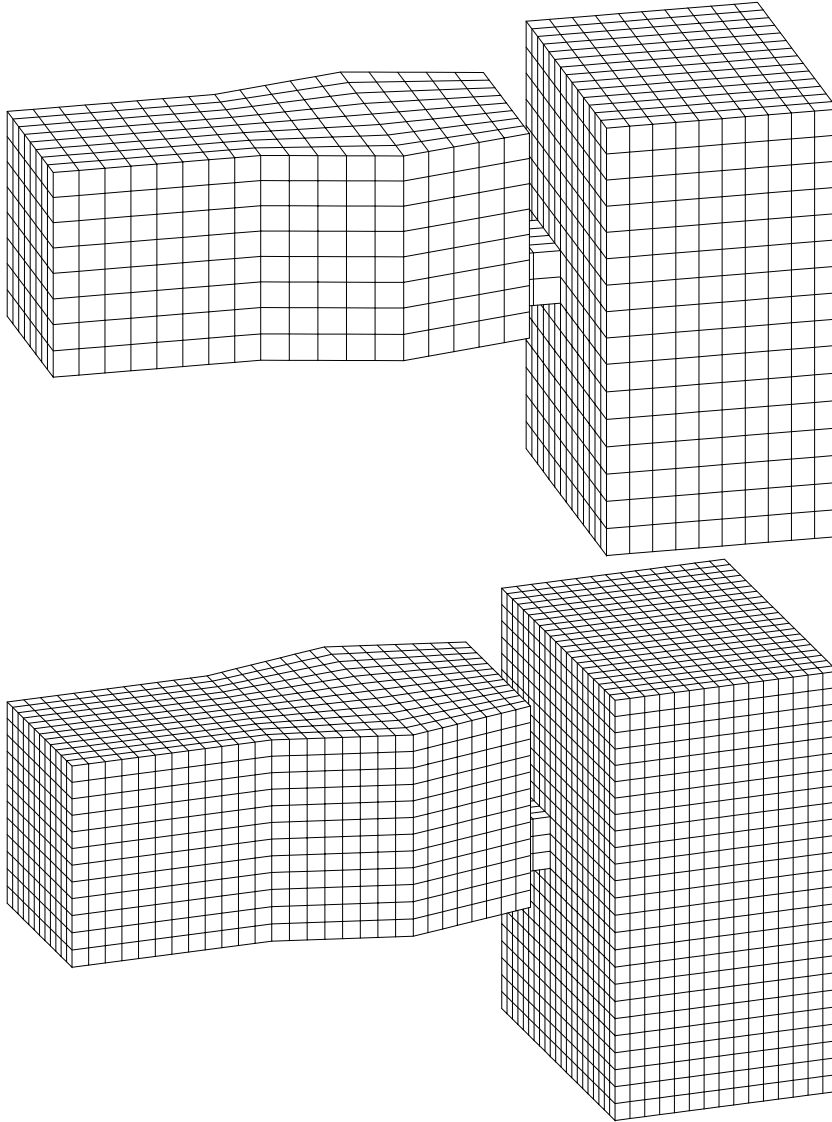


Figure 3: **HDR test E12.3.2 in 2D geometry.** Pressure histories corresponding to the coarse mesh (top) and the fine mesh (bottom). **The red line corresponds to the experimental results.**

3D version of the E12.3.2 computation.

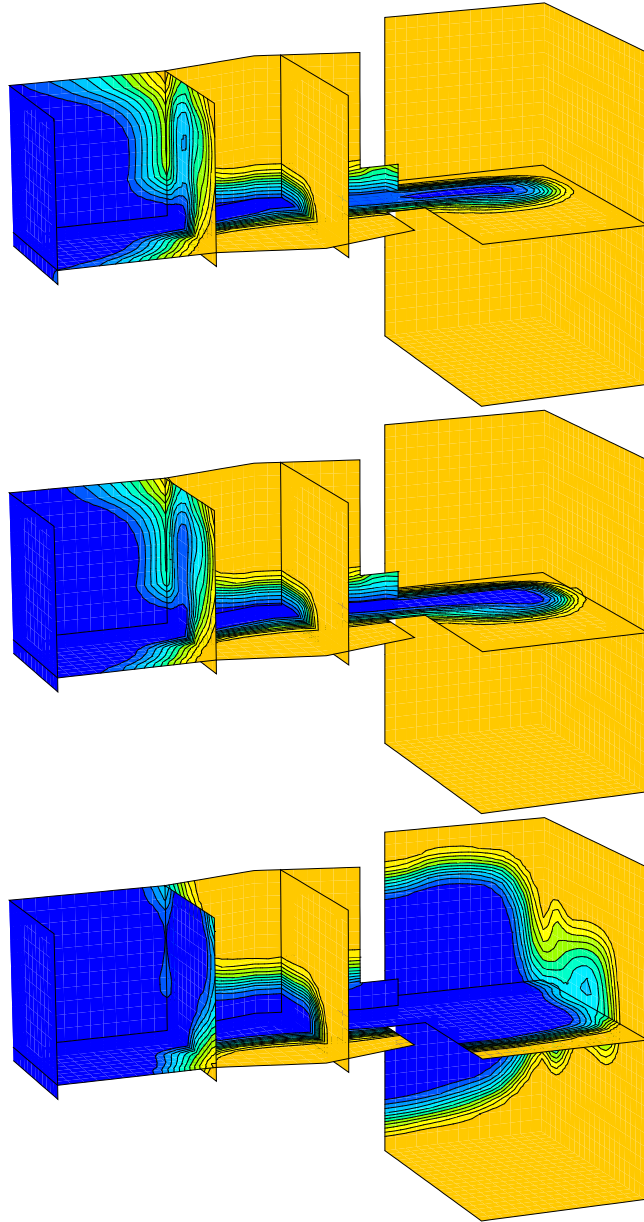
Mesh of 3 412 elements ($\Delta x \approx 0.55$ m) (top)

Mesh of 11 965 elements ($\Delta x \approx 0.37$ m) (bottom)



3D. Hydrogen Mass Fraction Evolution. Fine Mesh.

$t = 2.4$ s, $t = 2.5$ s and $t = 2.9$ s



3D. Pressure evolutions. Effect of the Grid Refinement.

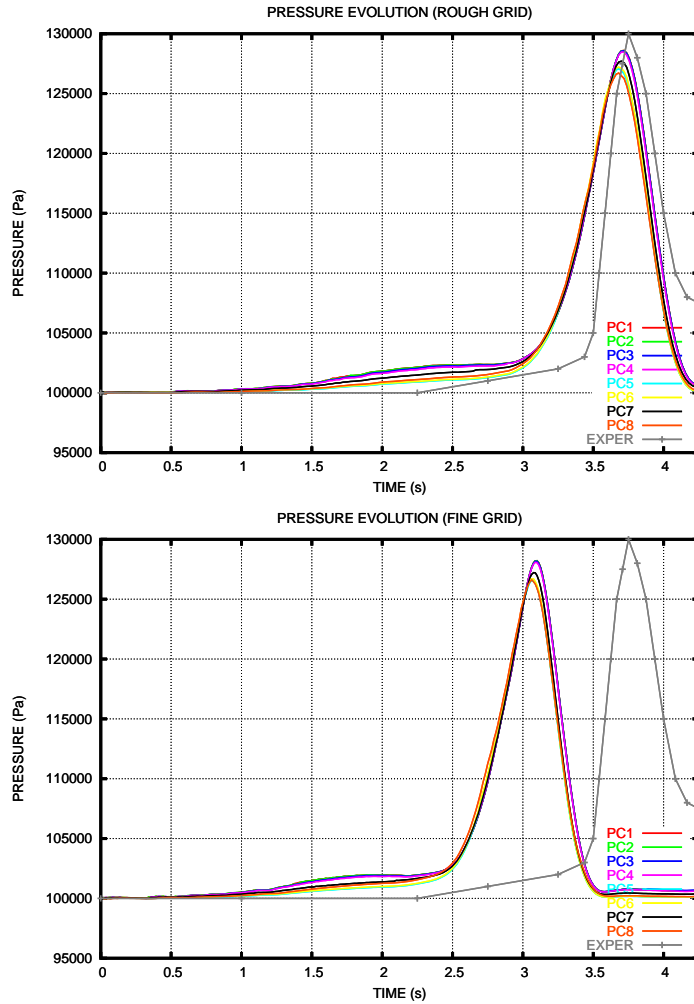


Figure 4: **HDR test E12.3.2 in 3D geometry**. Pressure histories corresponding to the coarse mesh (top) and the fine mesh (bottom). **The grey line corresponds to the experimental results.**

Hydrogen Deflagration Test Ex29.

Method	R7a	R7b	R5
I	12.86	13.04	18.13
II	11.4	11.4	11.4
III	33.6	33.6	33.6
3D, present comp.	0.265	25.0	20.0

Table 2: **BMC Test Ex29**. Values of K_0 obtained using different methods.

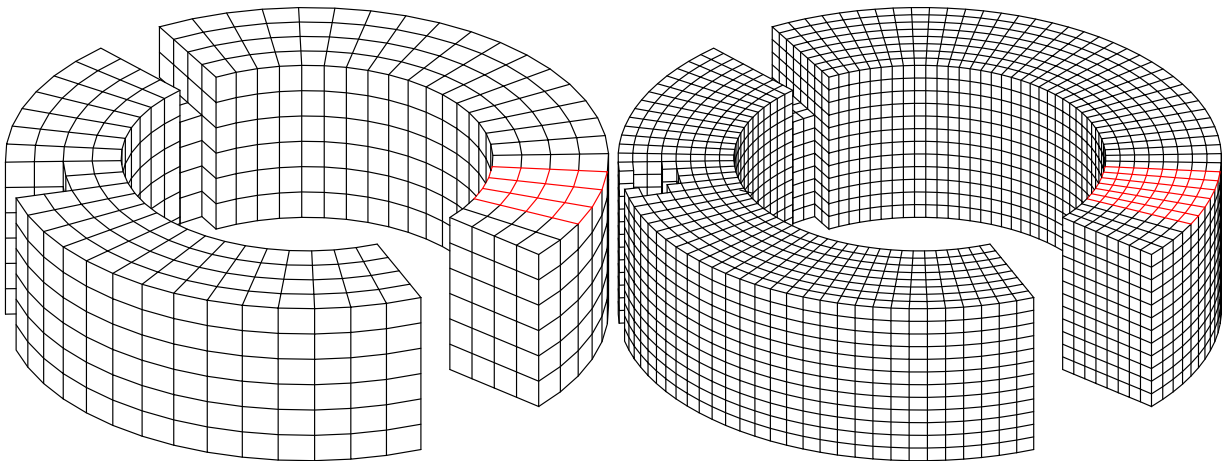
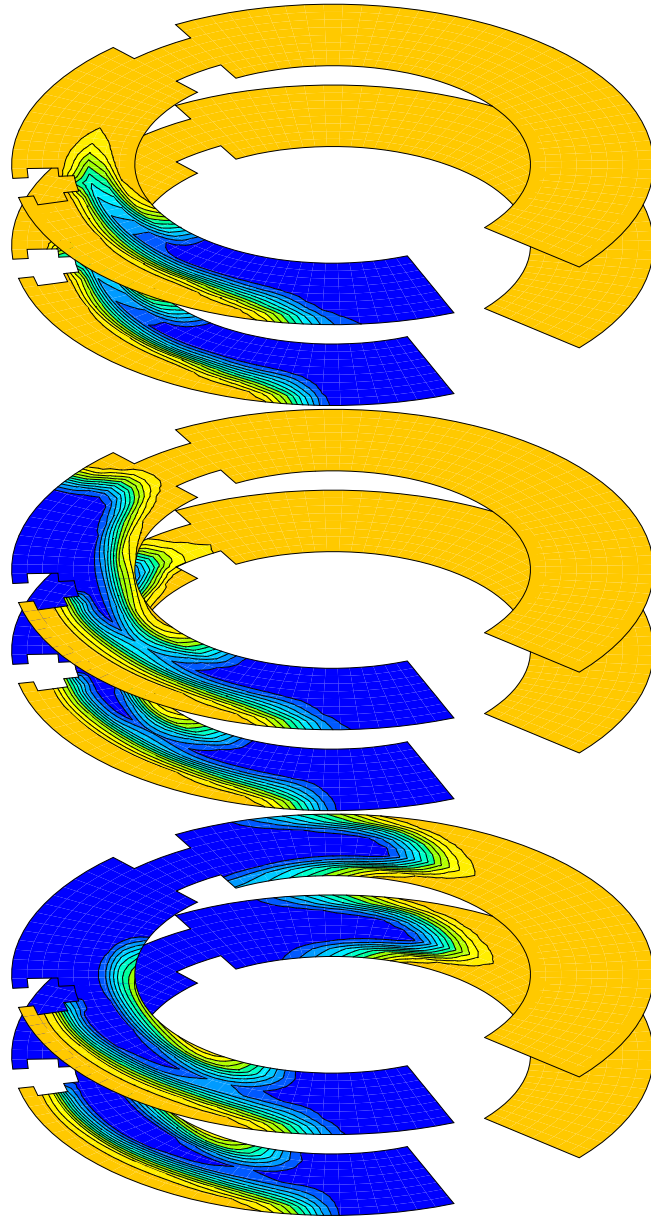


Figure 5: **BMC test Ex29 in 3D geometry**. Grid of 1098 elements (left; $\Delta x_{ave} = 0.41526$ m) and grid of 8832 elements (right; $\Delta x_{ave} = 0.2078$ m)

Hydrogen Deflagration Test Ex29.
Hydrogen Mass Fraction Isolines at
 $t = 2.875$ s, $t = 2.925$ s and $t = 2.95$ s



Hydrogen Deflagration Test Ex29.

Comparison with Experimental Results.

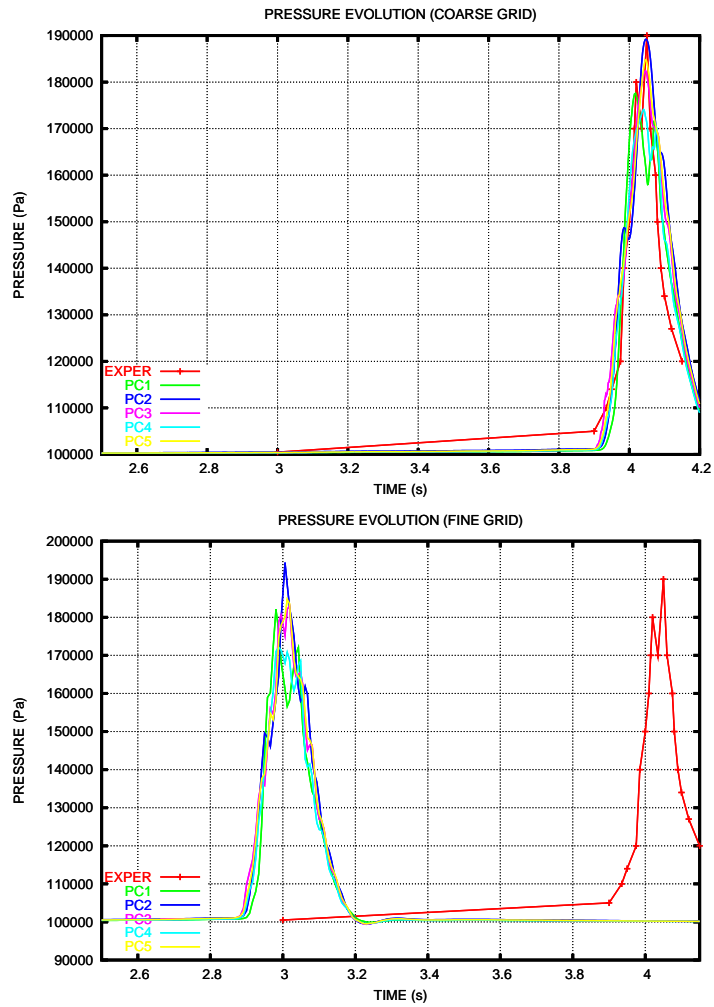


Figure 6: **BMC test Ex29 in 3D geometry.** Pressure histories corresponding the coarse mesh (left) and the fine mesh (right). **The red line corresponds to the experimental results.**